

Conexion D57 30/04/25

Ex 1

1°] $PV = nRT$

$n = \frac{N}{N_A}$ ← nombre de molécules
 $\uparrow$
 nb de moles.

$n^* = \frac{N}{V}$

$P = n^* \frac{R}{d_a} \cdot T = n^* P_B \cdot T = \frac{1}{3} n^* \cdot m \cdot u^2 \Rightarrow \boxed{u = \sqrt{\frac{3 P_B \cdot T}{m}}}$

2°] $\Pi = m \cdot d_a \Rightarrow \boxed{m = \frac{\Pi}{d_a}}$ AN $m = \frac{40 \cdot 10^{-3}}{6,02 \cdot 10^{23}} =$

d'a $\boxed{u = 182 \text{ ms}^{-1}}$

3°] a) $U_{\text{mol}} = (E_c)_{\text{mole}} = \sum \frac{1}{2} m v_i^2 = \frac{1}{2} m \sum v_i^2 = \frac{1}{2} m \cdot d_a u^2$
 $= \frac{1}{2} \cancel{n^*} d_a \cdot \frac{3 P_B \cdot T}{\cancel{m}} = \boxed{\frac{3}{2} RT = U_{\text{mol}}}$

b] $\frac{dU_{\text{mol}}}{dT} = \frac{3}{2} R = C_v$: capacité thermique à volume cst.
 Variation d'énergie interne quand T varie de 1K.

Ex 2

I.A Atmosphère isotherme.

1°] $PV = nRT_0 = \frac{m}{M_e} RT_0 \rightarrow \boxed{\rho = \frac{PM_e}{RT_0}}$

2°] $\square \vec{d}z$ dZ e eq $-g \rho dZ + \mu \vec{g} dZ = 0. \Rightarrow$

$\boxed{\vec{g} \rho dZ = \mu \vec{g}}$

projectée sur oz ascendant $\Rightarrow \frac{d\rho}{dz} = -\mu g = -\frac{\rho M_e g}{RT_0}$

$\boxed{\frac{d\rho}{dz} + \frac{\rho M_e g}{RT_0} = 0}$

On pose $H = \frac{RT_0}{M_e g} \Rightarrow \boxed{\rho = \rho_0 e^{-\frac{z}{H}}}$

3°] $\rho_{O_2} = 32 \text{ g mol}^{-1}$
 $\rho_{N_2} = 28 \text{ g mol}^{-1}$

$\rho_e = 20\% \rho_{O_2} + 80\% \rho_{N_2} = 28,8 \cdot 10^{-3} \text{ kg mol}^{-1}$
 $H = 8,5 \text{ km}$

$\rho = \rho_0 / 2 \Rightarrow -\frac{\rho_0}{H} = \frac{1}{2} \Rightarrow \boxed{z_{50\%} = H \cdot \ln 2}$

AN $\boxed{z_{50\%} = 5,9 \text{ km}}$

$$B) T = T_0(1 - \alpha z)$$

$$6) \frac{dP}{dz} + \frac{P \cdot \frac{d\alpha}{dz}}{R T_0(1 - \alpha z)} = 0 \Rightarrow \frac{dP}{P} = - \frac{dz}{H(1 - \alpha z)}$$

$$\text{d'où } \ln P = \frac{1}{\alpha H} \ln(1 - \alpha z) + \text{cte} \Rightarrow \ln \frac{P}{P_0} = \ln(1 - \alpha z)^{\frac{1}{\alpha H}}$$

$$\ln P_0 = 0 + \text{cte}$$

$$\Rightarrow \boxed{P = P_0 (1 - \alpha z)^{\beta}} \quad \text{avec } \boxed{\beta = \frac{1}{\alpha H} = \frac{z_0}{H}}$$

La loi des G.P donne :

$$\mu = \frac{P \cdot M}{R \cdot T} = \frac{P_0 (1 - \alpha z)^{\beta} \cdot M}{R T_0 (1 - \alpha z)} \Rightarrow \boxed{\mu = \mu_0 (1 - \alpha z)^{\beta - 1}}$$

$$5) P(z) = \frac{P_0}{2} \Rightarrow \frac{1}{2} = (1 - \alpha z)^{\beta} = 2^{-\frac{1}{\beta}} - 1 = -\alpha z_{50\%} \Rightarrow \boxed{z_{50\%} = z_0 \left(1 - 2^{-\frac{1}{\beta}}\right)}$$

$\Rightarrow \boxed{z_{50\%} = 5,4 \text{ km.}}$ Valeur proche de celle du modèle isotherme mais inférieure car $T \searrow$ lorsque $z \uparrow$.

6) Fig 2 $\rightarrow$ T fonction linéaire et de constante de z .

$$T(z=0) \approx 288 \text{ K.}$$

$$T = T_0 - T_0 \alpha \cdot z \Rightarrow T_0 \cdot \alpha = 6,94 \Rightarrow$$

$$= 288,14 - 6,94 \cdot z$$

$$\alpha = \frac{1}{z_0} = \frac{6,94}{288} \Rightarrow$$

$$\boxed{z_0 = \frac{288}{6,94} = 41,5 \text{ km.}}$$

$$P = P_0 (1 - \alpha z)^{\beta}$$

$$T = T_0 (1 - \alpha z) \Rightarrow P = P_0 \left(\frac{T}{T_0}\right)^{\beta}$$

$$= 1,01 \left(\frac{T}{288,08}\right)^{5,25}$$

$$\Rightarrow P_0 = 1,01 \text{ bar.}$$

$$\beta = 5,25 = \frac{z_0}{H} \Rightarrow \boxed{H = 7,9 \text{ km.}}$$

Valeurs proches.

7°) Atmosphère : $(P_e; \mu_e; T_e)$.

Volume du ballon $V_0 = 2000 \text{ m}^3$

$m = \text{masse nacelle + passagers} = 500 \text{ kg}$.

$m_i = \text{masse d'air chaud}$.

Intérieur du ballon $(P_i; T_i)$. $P_i = P_e$.

$$P_i V_0 = \frac{m_i}{\mu_e} R T_i \quad \text{et} \quad P_i = P_e \quad m_i = \frac{P_e V_0}{R T_i} \cdot \mu_e \quad \text{et} \quad \mu_e = \frac{P_e \cdot \mu_e}{R T_e}.$$

$$\boxed{m_i = \frac{T_e}{T_i} V_0 \cdot \mu_e.}$$

8°) A l'éq $\vec{F}_{\text{Arch}} + \vec{P}_{\text{poids}} = 0$ et projectée sur z ascendant.

$$\mu_e g V_0 - (m + m_i) g = 0. \quad \text{et} \quad m = \mu_e V_0 - m_i$$

$$\text{et} \quad \mu_e V_0 = m_i \cdot \frac{T_e}{T_i} \Rightarrow \boxed{m = m_i \left(\frac{T_i}{T_e} - 1 \right)}$$

9°) en $z = z_m$ $\vec{F}_{\text{Arch}} - m \vec{g} = 0$

$$\mu_e V_0 g = m g \Rightarrow m = V_0 \mu_e (1 - \alpha z_m)^{\beta-1}$$

$$\Rightarrow \boxed{z_m = \frac{1}{\alpha} \left(1 - \left(\frac{m}{V_0 \mu_e} \right)^{\frac{1}{\beta-1}} \right)} \quad \text{AN} \quad \boxed{z_m = 13 \text{ km.}}$$

10°) Calcul de T_i par l'éq. mécanique au sol:

$$m + m_i \leq \mu_e V_0 \Rightarrow m + \frac{T_e}{T_i} V_0 \mu_e \leq \mu_e V_0 \quad \text{avec} \quad T_e = T_0 \quad \mu_e = \mu_0.$$

$$m \leq \mu_e V_0 \left(1 - \frac{T_0}{T_i} \right) \Rightarrow 1 - \frac{T_0}{T_i} \geq \frac{m}{\mu_e V_0} \Rightarrow \frac{T_0}{T_i} \leq 1 - \frac{m}{\mu_e V_0}.$$

$$T_i \geq \frac{T_0}{1 - \frac{m}{\mu_e V_0}} \Rightarrow \boxed{T_d = \frac{T_0}{1 - \frac{m}{\mu_e V_0}}} \quad \text{AN} \quad T_d \geq 382 \text{ K.}$$

$$\text{Eq en } z \neq 0 \quad m + \frac{T_e}{T_i} \nu_0 \mu_e = \mu_e \nu_0$$

$$\text{Eq en } z = 0 \quad m + \frac{T_0}{T_d} \nu_0 \mu_0 = \mu_0 \nu_0$$

d'où en égalant les
2 valeurs de m :

$$\mu_e \left(1 - \frac{T_e}{T_i}\right) = \mu_0 \left(1 - \frac{T_0}{T_d}\right)$$

$$\text{et } \mu_e = \mu_0 (1 - \alpha z)^{\beta-1}$$

$$P_e = P_0 (1 - \alpha z)^{\beta}$$

$$T_e = T_0 (1 - \alpha z)$$

$$\mu_0 \frac{(1 - \alpha z)^{\beta}}{(1 - \alpha z)} \left(1 - \frac{T_e}{T_i}\right) = \mu_0 \left(1 - \frac{T_0}{T_d}\right)$$

$$\mu_0 \frac{P_e}{P_0 (1 - \alpha z)} \left(1 - \frac{T_e}{T_i}\right) = \mu_0 \left(1 - \frac{T_0}{T_d}\right)$$

$$\frac{P_e \cdot T_0}{P_0 T_e} \left(1 - \frac{T_e}{T_i}\right) = 1 - \frac{T_0}{T_d} \Rightarrow$$

$$\left| P_e \left(\frac{1}{T_e} - \frac{1}{T_i} \right) = P_0 \left(\frac{1}{T_0} - \frac{1}{T_d} \right) \right|$$

Ex 3.

Ex 3

$$36) \left. \begin{aligned} C_p - C_v &= nR \\ \gamma &= \frac{C_p}{C_v} \end{aligned} \right\} \rightarrow$$

$$C_v = \frac{nR}{\gamma - 1}$$

$$C_p = \frac{nR\gamma}{\gamma - 1}$$

$$\text{ou } P_0 V_A = nRT_0 \Rightarrow$$

$$C_v = \frac{P_0 V_A}{T_0 (\gamma - 1)}$$

$$C_p = \frac{P_0 V_A \cdot \gamma}{T_0 (\gamma - 1)}$$

37) de 0 $\rightarrow$ 1 la cage reste en contact avec A

donc le volume ne varie pas. La transformation est isochore.

38) la poutre est à l'équilibre ds l'état 1: $\vec{P}_{\text{poutre}} + \vec{F}_{\text{gaz/poutre}} + \vec{F}_{\text{atm/poutre}} = \vec{0}$

$$\Rightarrow (mg - P_1 S + P_0 S) \vec{e}_z = \vec{0} \Rightarrow P_1 = P_0 + \frac{mg}{S}$$

$$P_0 V_A = nRT_0$$

$$P_1 V_A = nRT_1$$

$$\Rightarrow \frac{P_1}{P_0} = \frac{T_1}{T_0} \rightarrow T_1 = T_0 \cdot \frac{P_1}{P_0} \Rightarrow$$

$$T_1 = T_0 \left(\frac{P_0 + \frac{mg}{S}}{P_0} \right)$$

AN $T_1 = 330 \text{ K}$
330K.

(2)

(4)

39) $\Delta U_{0 \rightarrow 1} = Q_{0 \rightarrow 1} + \underbrace{W_{0 \rightarrow 1}}_{=0}$ car la transformation est isochore.

$$Q_{0 \rightarrow 1} = m C_V (T_1 - T_0) = \frac{mR}{\gamma - 1} (T_1 - T_0) = \boxed{\frac{P_0 V_A}{\gamma - 1} \left(\frac{T_1}{T_0} - 1 \right) = Q_{0 \rightarrow 1}}$$

AN $\boxed{Q_{0 \rightarrow 1} = 8,25 \text{ J}}$

40] de 1 à 2, $\boxed{P_{\text{gaz}} = P_1 = P_0 + \frac{mg}{S} = P_2}$ (On chauffe très doucement donc les variables d'état restent définies) $\Rightarrow$ Transformation isobare

41] $P_1 V_A = m R T_1$
 $P_1 V_B = m R T_2 \Rightarrow \frac{T_2}{T_1} = \frac{V_B}{V_A} \Rightarrow \boxed{T_2 = T_1 \cdot \frac{V_B}{V_A}}$

AN $\boxed{T_2 = 1000 \text{ K}}$

42] $\Delta H_{1 \rightarrow 2} = Q_{1 \rightarrow 2} = m C_P (T_2 - T_1) = \frac{mR\gamma}{\gamma - 1} \Delta T = \boxed{\frac{P_0 V_A \cdot \gamma}{T_0 (\gamma - 1)} (T_2 - T_1)}$

AN $\boxed{Q_{1 \rightarrow 2} = 260 \text{ J}}$

43] 2 $\rightarrow$ 3 la cage reste en B la transformation est isochore quasi statique

et $P_3 = P_0$ et $P_3 V_B = P_0 V_B = m R T_3 \Rightarrow \frac{T_3}{T_2} = \frac{P_0}{P_2} \Rightarrow$
 $P_2 V_B = m R T_2$

$$\boxed{T_3 = T_2 \cdot \frac{P_0}{P_1}}$$

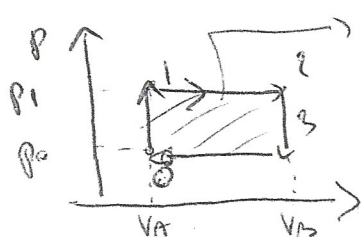
3 $\rightarrow$ 0 Transformation isobare à $P_3 = P_0$.

44] $W_{\text{cycle}} = W_{0 \rightarrow 1} + W_{1 \rightarrow 2} + W_{2 \rightarrow 3} + W_{3 \rightarrow 0}$

$$= 0 + -P_1 (V_B - V_A) + 0 - P_0 (V_A - V_B) = V_B (P_0 - P_1) + V_A (P_1 - P_0) = (V_B - V_A) [P_0 - P_1] = \boxed{-\frac{mg}{S} (V_B - V_A)}$$

AN $\boxed{W = -6,7 \text{ J}}$ Re $W_{\text{gaz}} < 0 \Rightarrow$ cycle moten

45+46]



Anc = $|W_{\text{cycle}}|$

cycle decrit ds le sens horaire donc $\boxed{W < 0}$ et

Anc du cycle = $(P_1 - P_0) \cdot (V_B - V_A)$

(5) $\eta = \frac{-W}{Q_{0 \rightarrow 1}}$

1) Préliminaires.

1) $H_S = U_S + P \cdot V$

2) $\Delta H_S = \Delta U_S + \Delta(PV) = \Delta U_S + P_{ext} \Delta V$ puisque $P_S = P_{ext}$.

ou $\Delta H_S = W_S + Q_{ext}$ et $W_S = -P_{ext} \Delta V$

d'où $\Delta H_S = Q_{ext}$.

3) $dH_S = m c dT = \delta Q_{ext}$.

II de mélange est thermiquement isolé.

à $t=0$ $T = T_{ext}$.

1) $\Delta H = Q_{ext} = m c (T_1 - T_{ext})$ so.

2) or $\Delta H = Q_{ext} = P_R \Delta t$.

d'où $\Delta t = \frac{m c (T_1 - T_{ext})}{P_R}$.

AN $m = 100 \text{ kg}$
 $c = 38 \cdot 10^3 \text{ J kg}^{-1} \text{ K}^{-1}$
 $T_{ext} = 290 \text{ K}$
 $T_1 = 350 \text{ K}$
 $P_R = 15 \cdot 10^3 \text{ W}$

$Q_{ext} = 100 \cdot 38 \cdot 10^3 (350 - 290) = 2.3 \cdot 10^7 \text{ J}$.

$\Delta t = \frac{2.3 \cdot 10^7}{15 \cdot 10^3} = 1556 \text{ s} = 4,6 \text{ h}$

III Perte thermique.

$\delta Q_p = -k (T - T_{ext}) dt$

ou $\frac{dT}{dt} = -\frac{k}{m c} (T - T_{ext})$

so $\frac{dT}{T - T_{ext}} = -\frac{k}{m c} dt$

on $\int_{T_{ext}}^{T_1} \frac{dT}{T - T_{ext}} = -\frac{k}{m c} \int_0^{\Delta t} dt$

En régime permanent $dH_{eq} = 0$ puisque $T = T_{eq} = \text{cte}$.

d'où $dH_{eq} = P_R dt - k (T_{eq} - T_{ext}) dt = 0$.

AN $T_{eq} = 290 \text{ K}$ $P_R = 15 \cdot 10^3 \text{ W}$
 $T_{eq} = 290 \text{ K}$

$\Rightarrow P_R = \frac{15 \cdot 10^3}{80} = 18,8 \text{ W K}^{-1} = k$.

(3)

2) Le chauffage est actif.

à $t=0$, $T = T_{ext}$.

2) $dH_{eq} = m c dT = -k (T - T_{ext}) dt$.

$\Rightarrow m c \frac{dT}{dt} + k T = k T_{ext} \Rightarrow \frac{dT}{dt} + \frac{k}{m c} T = \frac{k}{m c} T_{ext}$.

$Z = \frac{k}{m c}$.

$T(t) = A e^{-\frac{k}{m c} t} + T_{ext}$

à $t=0$ $T_{lim} = A + T_{ext} \Rightarrow A = T_{lim} - T_{ext}$.

$T(t) = (T_{lim} - T_{ext}) e^{-\frac{k}{m c} t} + T_{ext}$.



3) Partir en température de la même d'eau - $t=0$ $T = T_{ext}$.

$m c dT = P_R dt - k (T - T_{ext}) dt$.

$\Rightarrow m c \frac{dT}{dt} + k T = P_R + k T_{ext}$.

$T(t) = A e^{-\frac{k}{m c} t} + \frac{P_R}{k} + T_{ext}$.

à $t=0$ $T(t) = T_{ext} = A + \frac{P_R}{k} + T_{ext} \Rightarrow A = -\frac{P_R}{k}$.

$T(t) = -\frac{P_R}{k} e^{-\frac{k}{m c} t} + \frac{P_R}{k} + T_{ext}$.

pour $\Delta t = t_1$ $T = T_1$.

$T_1 = -\frac{P_R}{k} e^{-\frac{k}{m c} t_1} + \frac{P_R}{k} + T_{ext}$.

$\Rightarrow (T_1 - T_{ext} - \frac{P_R}{k}) e^{\frac{k}{m c} t_1} = -\frac{P_R}{k} e^{-\frac{k}{m c} t_1}$

(4)

$t_1 = -\frac{m c}{k} \ln \left(1 - \frac{k}{P_R} (T_1 - T_{ext}) \right)$.

AN $t_1 = 8,6 \text{ h}$.